# **Real-Time Optimization (RTO)**

- In previous chapters we have emphasized control system performance for disturbance and set-point changes.
- Now we will be concerned with how the set points are specified.
- In *real-time optimization (RTO)*, the optimum values of the set points are re-calculated on a regular basis (e.g., every hour or every day).
- These repetitive calculations involve solving a constrained, steady-state optimization problem.

#### • Necessary information:

- 1. Steady-state process model
- 2. Economic information (e.g., prices, costs)
- 3. A *performance Index* to be maximized (e.g., profit) or minimized (e.g., cost).
  - **Note:** Items # 2 and 3 are sometimes referred to as an *economic model.*

#### Process Operating Situations That Are Relevant to Maximizing Operating Profits Include:

- 1. Sales limited by production.
- 2. Sales limited by market.
- 3. Large throughput.
- 4. High raw material or energy consumption.
- 5. Product quality better than specification.
- 6. Losses of valuable or hazardous components through waste streams.

# **Common Types of Optimization Problems**

#### **1. Operating Conditions**

- Distillation column reflux ratio
- Reactor temperature

#### 2. Allocation

- Fuel use
- Feedstock selection

#### 3. Scheduling

- Cleaning (e.g., heat exchangers)
- Replacing catalysts
- Batch processes



# Figure 19.1 Hierarchy of process control activities.

#### BASIC REQUIREMENTS IN REAL-TIME OPTIMIZATION

#### **Objective Function:**

$$\boldsymbol{P} = \sum_{s} \boldsymbol{F}_{s} \boldsymbol{V}_{s} - \sum_{r} \boldsymbol{F}_{r} \boldsymbol{C}_{r} - \boldsymbol{O} \boldsymbol{C}$$
(19-1)

where: *P* = operating profit/time

 $\sum_{s} F_{s}V_{s} = \text{sum of (product flow rate) x (product value)}$   $\sum_{r} F_{r}C_{r} = \text{sum of (feed flow rate) x (unit cost)}$  OC = operating costs/time

# Both the operating and economic models typically will include constraints on:

- 1. **Operating Conditions**
- 2. Feed and Production Rates
- 3. Storage and Warehousing Capacities
- 4. **Product Impurities**

#### The Interaction Between Set-point Optimization and Process Control

#### **Example: Reduce Process Variability**

- Excursions in chemical composition => off-spec products and a need for larger storage capacities.
- Reduction in variability allows set points to be moved closer to a limiting constraint, e.g., product quality.





Figure 19.2 A block diagram for RTO and regulatory feedback control.

# The Formulation and Solution of RTO Problems

- 1. The economic model: An objective function to be maximized or minimized, that includes costs and product values.
- 2. The operating model: A steady-state process model and constraints on the process variables.

# The Formulation and Solution of RTO Problems

# Table 19.1 Alternative Operating Objectives for a FluidizedCatalytic Cracker

- 1. Maximize gasoline yield subject to a specified feed rate.
- 2. Minimize feed rate subject to required gasoline production.
- 3. Maximize conversion to light products subject to load and compressor/regenerator constraints.
- 4. Optimize yields subject to fixed feed conditions.
- 5. Maximize gasoline production with specified cycle oil production.
- 6. Maximize feed with fixed product distribution.
- 7. Maximize FCC gasoline plus olefins for alkylate.

# **Selection of Processes for RTO**

#### **Sources of Information for the Analysis:**

#### 1. Profit and loss statements for the plant

- Sales, prices
- Manufacturing costs etc.

#### 2. Operating records

- Material and energy balances
- Unit efficiencies, production rates, etc.

#### **Categories of Interest:**

- 1. Sales limited by production
  - Increases in throughput desirable
  - Incentives for improved operating conditions and schedules.

#### 2. Sales limited by market

- Seek improvements in efficiency.
- Example: Reduction in manufacturing costs (utilities, feedstocks)
- 3. Large throughput units
  - Small savings in production costs per unit are greatly magnified.

## The Formulation and Solution of RTO Problems

- Step 1. Identify the process variables.
- Step 2. Select the objective function.
- Step 3. Develop the process model and constraints.
- Step 4. Simplify the model and objective function.
- Step 5. Compute the optimum.
- Step 6. Perform sensitivity studies.

#### Example 19.1

A section of a chemical plant makes two specialty products (E, F) from two raw materials (A, B) that are in limited supply. Each product is formed in a separate process as shown in Fig. 19.3. Raw materials A and B do not have to be totally consumed. The reactions involving A and B are as follows:

	Process	1:	1.1	A +	<b>B</b>	> E
•	Process	2:		<b>A</b> +	2 <b>B</b> -	→F

The processing cost includes the costs of utilities and supplies. Labor and other costs are 200/day for process 1 and 350/day for process 2. These costs occur even if the production of E or F is zero. Formulate the objective function as the total operating profit per day. List the equality and inequality constraints (Steps 1, 2, and 3).

**Available Information** 

F

2

	Max Raw Material	timum Available (lb/day)	Cost (¢/15)	
	A B <sub>/</sub>	40,000 30,000	15 20	1
Process Prod	Reactant Requirements (lb) per lb uct Product	Processing Cost	Selling Price of Product	Maximum Production Level (lb/day)
1 E	2/3 A, 1/3 B	15 ¢/lb E	40 ¢/lb E	30.000

SOLUTION

The optimization problem is formulated using the first three steps delineated above.

1/2 A, 1/2 B

Step 1. The relevant process variables are the mass flow rates of reactants and products (see Fig. 19.3):

5¢/lbF

 $x_1 = lb/day A$  consumed  $x_2 = lb/day B$  consumed  $x_3 = lb/day E produced$  $x_4 = lb/day F produced$ 

Step 2. In order to use Eq. 19-1 to compute the operating product per day, we need to spec-ify product sales income, feedstock costs, and operating costs: 目前的:

Sales income 
$$(\frac{day}{day}) = \sum_{s} F_{s} V_{s} = 0.4x_{3} + 0.33x_{4}$$
 (19-2)

Feedstock costs (\$/day) = 
$$\sum_{r} F_r C_r = 0.15x_1 + 0.2x_2$$
 (19-3)

Operating costs 
$$(\frac{day}{day}) = OC = 0.15x_3 + 0.05x_4 + 350 + 200$$
 (19-4)

Substituting into (19-1) yields the daily profit:

$$P = 0.4x_3 + 0.33x_4 - 0.15x_1 - 0.2x_2 - 0.15x_3 - 0.05x_4 - 350 - 200$$
  
= 0.25x\_3 + 0.28x\_4 - 0.15x\_1 - 0.2x\_2 - 550 (19-5)

Step 3. Not all variables in this problem are unconstrained. First consider the material balance equations, obtained from the reactant requirements, which in this case comprise the process operating model: 化油水的 化口口

$$x_1 = 0.667x_3 + 0.5x_4 \tag{19-6a}$$

33 ¢/lb F

$$x_2 = 0.333x_3 + 0.5x_4 \tag{19-6b}$$

Ł

30,000

The limits on the feedstocks and production levels are:

$0 \le x_1 \le 40,000$	(19-7a)
$0 \le x_2 \le 30,000$	(19-7b)
$0 \le x_3 \le 30,000$	( <b>19-7</b> c)
$0 \le x_4 \le 30,000$	(19-7d)

Equations (19-5) through (19-7) constitute the optimization problem to be solved. Because the variables appear linearly in both the objective function and constraints, this formulation is referred to as a *linear programming problem*, which is discussed in Section 19.4.

#### **UNCONSTRAINED OPTIMIZATION**

- The simplest type of problem
- No inequality constraints
- An equality constraint can be eliminated by variable substitution in the objective function.

# **Single Variable Optimization**

• A single independent variable maximizes (or minimizes) an objective function.

#### • Examples:

- 1. Optimize the reflux ratio in a distillation column
- 2. Optimize the air/fuel ratio in a furnace.
- Typical Assumption: The objective function f (x) is unimodal with respect to x over the region of the search.
  - Unimodal Function: For a maximization (or minimization) problem, there is only a single maximum (or minimum) in the search region.

#### **Different Types of Objective Functions**



Figure 19.5 Three types of optimal operating conditions.

### **One Dimensional Search Techniques**

Selection of a method involves a trade-off between the number of objective function evaluations (computer time) and complexity.

#### 1. "Brute Force" Approach

Small grid spacing ( $\Delta x$ ) and evaluate f(x) at each grid point  $\Rightarrow$  can get close to the optimum but very inefficient.

#### 2. Newton's Method

- It is based on the necessary condion for optimality: f'(x)=0.
- **Example:** Find a minimum of f(x). Newton's method gives,

$$x^{k+1} = x^k - \frac{f'(x^k)}{f''(x^k)}$$

#### 3. Quadratic Polynomial fitting technique

- 1. Fit a quadratic polynomial,  $f(x) = a_0 + a_1 x + a_2 x^2$ , to three data points in the interval of uncertainty.
  - Denote the three points by  $x_a$ ,  $x_b$ , and  $x_c$ , and the corresponding values of the function as  $f_a$ ,  $f_b$ , and  $f_c$ .
- 2. Find the optimum value of *x* for this polynomial:

$$\boldsymbol{x}^{*} = \frac{1}{2} \frac{\left(\boldsymbol{x}_{b}^{2} - \boldsymbol{x}_{c}^{2}\right) \boldsymbol{f}_{a} + \left(\boldsymbol{x}_{c}^{2} - \boldsymbol{x}_{a}^{2}\right) \boldsymbol{f}_{b} + \left(\boldsymbol{x}_{a}^{2} - \boldsymbol{x}_{b}^{2}\right) \boldsymbol{f}_{c}}{\left(\boldsymbol{x}_{b} - \boldsymbol{x}_{c}\right) \boldsymbol{f}_{a} + \left(\boldsymbol{x}_{c} - \boldsymbol{x}_{a}\right) \boldsymbol{f}_{b} + \left(\boldsymbol{x}_{a} - \boldsymbol{x}_{b}\right) \boldsymbol{f}_{c}}$$
(19-8)

- 4. Evaluate  $f(x^*)$  and discard the x value that has the <u>worst</u> value of the objective function. (i.e., discard either  $x_a$ ,  $x_b$ , or  $x_c$ ).
- 5. Choose  $x^*$  to serve as the new, third point.
- 6. Repeat Steps 1 to 5 until no further improvement in  $f(x^*)$  occurs.



Figure 20.3. Two cases arising in a three-point equal-interval search.

#### **Case 1:** The maximum lies in $(x_2, b)$ .

**Case 2:** The maximum lies in  $(x_1, x_3)$ .

Chapter 19

# **Multivariable Unconstrained Optimization** $f(\mathbf{x}) \quad f(x_1, x_2, ..., x_{N_v})$

- Computational efficiency is important when *N* is large.
- "Brute force" techniques are not practical for problems with more than 3 or 4 variables to be optimized.
- **Typical Approach:** Reduce the multivariable optimization problem to a series of one dimensional problems:
  - (1) From a given starting point, specify a search direction.
  - (2) Find the optimum along the search direction, i.e., a one-dimensional search.
  - (3) Determine a new search direction.
  - (4) Repeat steps (2) and (3) until the optimum is located

#### • Two general categories for MV optimization techniques:

- (1) Methods requiring derivatives of the objective function.
- (2) Methods that do not require derivatives.

#### **Constrained Optimization Problems**

- Optimization problems commonly involve equality and inequality constraints.
- Nonlinear Programming (NLP) Problems:
  - a. Involve nonlinear objective function (and possible nonlinear constraints).
  - b. Efficient off-line optimization methods are available (e.g., conjugate gradient, variable metric).
  - c. On-line use? May be limited by computer execution time and storage requirements.

#### • Quadratic Programming (QP) Problems:

- a. Quadratic objective function plus linear equality and inequality constraints.
- b. Computationally efficient methods are available.
- Linear Programming (QP) Problems:
  - a. Both the objective function and constraints are
  - b. Solutions are highly structured and can be rapidly obtai

#### LP Problems (continued)

- Most LP applications involve more than two variables and can involve 1000s of variables.
- So we need a more general computational approach, based on the Simplex method.
- There are many variations of the Simplex method.
- One that is readily available is the Excel Solver.

#### **Recall the basic features of LP problems:**

- Linear objective function
- Linear equality/inequality constraints

#### Linear Programming (LP)

- Has gained widespread industrial acceptance for on-line optimization, blending etc.
- Linear constraints can arise due to:
  - **1. Production limitation:** e.g. equipment limitations, storage limits, market constraints.
  - 2. Raw material limitation
  - **3. Safety restrictions:** e.g. allowable operating ranges for temperature and pressures.
  - 4. Physical property specifications: e.g. product quality constraints when a blend property can be calculated as an average of pure component properties:

$$\overline{P} = \sum_{i=1}^n y_i P_i \leq \alpha$$

#### 5. Material and Energy Balances

- Tend to yield equality constraints.
- Constraints can change frequently, e.g. daily or hourly.

#### • Effect of Inequality Constraints

- Consider the linear and quadratic objective functions on the next page.
- Note that for the LP problem, the optimum must lie on one or more constraints.

#### Solution of LP Problems

- Simplex Method
- Examine only constraint boundaries
- Very efficient, even for large problems

#### **Linear Programming Concepts**

#### • For a linear process model,

$$y = Ku \tag{19-18}$$

The standard linear programming (LP) problem can be stated as follows:

minimize 
$$f = \sum_{i=1}^{N_V} c_i x_i$$
 (19-19)

subject to:

$$x_i \ge 0$$
  $i = 1, 2, ... N_V$   
 $\sum_{j=1}^{N_V} a_{ij} x_j \ge b_i$   $i = 1, 2, ... N_I$  (19-20)  
NV

$$\sum_{i=1}^{NY} \widetilde{a}_{ij} x_j = d_i \quad i = 1, 2, \dots N_E$$
 (19-21)





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**Figure 19.6** Operating window for a  $2 \ge 2$  optimization problem. The dashed lines are objective function contours, increasing from left to right. The maximum profit occurs where the profit line intersects the constraints at vertex D.



		y recus and riout	
	Volume pe	Maximum allowable production	
	Crude #1	Crude #2	(bbl/day)
Gasoline	80	44	24,000
Kerosene	5	10	2,000
Fuel oil	10	36	6,000
Processing cost (\$/bbl)	0.50	1.00	·

#### Table 19.3 Data for the Refinery Feeds and Products

**Solution** 

Let 
$$x_1 = crude \#1$$
 (bbl/day)  
 $x_2 = crude \#2$  (bbl/day)

Maximize profit (minimize cost):

y = income - raw mat'l cost - proc.cost

Calculate amounts of each product produced:

gasoline	 $0.80 x_1 + 0.44 x_2$
kerosene	 $0.05 x_1 + 0.10 x_2$
fuel oil	$0.10 x_1 + 0.36 x_2$
residual	$0.05 x_1 + 0.10 x_2$

#### Income

gasoline	$(36)(0.80 x_1 + 0.44 x_2)$
kerosene	$(24)(0.05 x_1 + 0.10 x_2)$
fuel oil	$(21)(0.10 x_1 + 0.36 x_2)$
residual	$(10)(0.05 x_1 + 0.10 x_2)$

Income =  $32.6 x_1 + 26.8 x_2$ Raw mat'l cost =  $24 x_1 + 15 x_2$ Processing cost =  $0.5 x_1 + x_2$ Then, the objective function is Profit = y =  $8.1 x_1 + 10.8 x_2$ 

#### **Constraints**

Maximum allowable production:  $0.80 x_1 + 0.44 x_2 \le 24,000$  (gasoline)  $0.05 x_1 + 0.10 x_2 \le 2,000$  (kerosene)  $0.10 x_1 + 0.36 x_2 \le 6,000$  (fuel oil) and, of course,  $x_1 \ge 0$ ,  $x_2 \ge 0$ 

## Graphical Solution

- 1. Plot constraint lines on  $x_1-x_2$  plane.
- 2. Determine feasible region (those values of  $x_1$  and  $x_2$  that satisfy maximum allowable production constraints.
- 3. Find point or points in feasible region that maximize  $y = 8.1 x_1 + 10.8 x_2$ ; this can be found by plotting the line  $8.1 x_1 + 10.8 x_2 = P$ , where P can vary, showing different profit levels.



**Chapter 19** 

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Chapter 19

Feasible Region With Parameterization of Objective Function in Linear Programming From the graph,

 $x_1^{opt} \sim 26,000$  $x_2^{opt} \sim 7,000$ 

More precisely, this is the intersection of the first two constraints, so  $x_1^{opt}$  and  $x_2^{opt}$  can be solved for simultaneously:

0.80 x1 + 0.44 x2 = 34,0000.50 x1 + 0.10 x2 = 2,000

 $\Rightarrow \dot{x}_1^{opt} = 26,200 \text{ and } x_2^{opt} = 6,900$ 

with P = \$286,740/day

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As expected, optimum is at a corner of the feasible region.

Investigate the profit at the other corners: Profit  $(x_1, x_2)$ 180,000 (0, 16667)(15000, 12500)256,500 (30000,0)243,000

# **Chapter 19**

#### QUADRATIC AND NONLINEAR PROGRAMMING

• The most general optimization problem occurs when both the objective function and constraints are nonlinear, a case referred to as nonlinear programming (NLP).

• The leading constrained optimization methods include:

- 1. Quadratic programming
- 2. Generalized reduced gradient
- 3. Successive quadratic programming (SQP)
- 4. Successive linear programming (SLP)

#### **Quadratic Programming**

- A quadratic programming problem minimizes a quadratic function of *n* variables subject to *m* linear inequality or equality constraints.
- In compact notation, the quadratic programming problem is

Minimize 
$$f(x) = c^T x + \frac{1}{2} x^T Q x$$
 (19-31)  
Subject to  $Ax = b$   
 $x \ge 0$  (19-32)

where c is a vector (n x 1), A is an m x n matrix, and Q is a symmetric n x n matrix.

#### **Nonlinear Programming**

 $\begin{array}{ll} \text{maximize} & f(x_1, x_2, \dots, x_{N_V}) & (19-13) \\ \text{subject to:} & h_i(x_1, x_2, \dots, x_{N_V}) = 0 & (i = 1, \dots, N_E) \\ & g_i(x_1, x_2, \dots, x_{N_V}) \le 0 & (i = 1, \dots, N_I) \end{array} \tag{19-13} \\ \end{array}$ 

- a) Constrained optimum: The optimum value of the profit is obtained when  $x=x_a$ . Implementation of an active constraint is straight-forward; for example, it is easy to keep a value closed.
- **b)** Unconstrained flat optimum: In this case the profit is insensitive to the value of *x*, and small process changes or disturbances do not affect profitability very much.
- **c) Unconstrained sharp optimum:** A more difficult problem for implementation occurs when the profit is sensitive to the value of *x*. If possible, we may want to select a different input variable for which the corresponding optimum is flatter so that the operating range can be wider.

#### **Nonlinear Programming (NLP) Example**

- nonlinear objective function
- nonlinear constraints



Figure 19.9 The allocation of two fuels in a boilerhouse with two turbine generators  $(G_1, G_2)$ .